

"Capacity Building and Strengthening Institutional Arrangement"

Workshop: Quantitative risk assessment of oil and gas plants

# APAT Experiences on Tools for Assessing Risks Preventing Accidents

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## APAT

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# Italian methodologies for major hazards quantitative risk assessment

## Hazards identification in industrial risk assessment



# THE RISK IDENTIFICATION METHODOLOGIES MAY BE SUBDIVIDED INTO THE FOLLOWING FOUR CATEGORIES :

- HISTORICAL ANALYSIS
- CHECK LIST
- STRUCTURED TECHNIQUES
- ( INDEX TECHNIQUES )



# THE HISTORICAL ANALYSIS IS BASED ON THE FOLLOWING SOURCES OF INFORMATION:

- PLANT OPERATING EXPERIENCE
- ACCIDENT DATA BANKS
- SPECIALIZED LITERATURE
- PRESS

THREE DIFFERENT TYPES OF CHECK-LISTS ARE NORMALLY USED:

- GENERAL (CONSISTING IN A WIDE SURVEY OF THE GENERAL PROBLEMS RELATED TO THE SAFETY). THEY MAY BE SUBDIVIDED:
  - FOR EVENTS AT THE BATTERY LIMITS OF THE UNIT BEING EXAMINED
    - · CAUSES EXTERNAL TO THE WORKS
    - CAUSES INTERNAL TO THE WORKS
  - FOR EVENTS INTERNAL TO THE UNIT BEING EXAMINED

THE CHECK LISTS BELONGING TO THIS TYPE ARE VERY QUICK TO APPLY, BUT NORMALLY QUITE SHALLOW, AND THEIR USEFULNESS IS CONSEQUENTLY LIMITED.



 DETAILED (FOR INSTANCE, THE ONES PROPOSED BY THE AIChE), DEALING WITH ALL THE SINGLE ASPECTS RELEVANT TO THE SAFETY OF THE PLANT, ITEM BY ITEM, FROM SEVERAL POINTS OF VIEW (DESIGN, OPERATION, MAINTENANCE, ETC.).

CHECK-LISTS OF THIS TYPE MAY BE VERY ONEROUS, AT THE SAME LEVEL OF SOME STRUCTURED TECHNIQUE. AT THE SAME TIME THEY WILL NOT GIVE EQUIVALENT ANALYTICAL AND CREATIVE CAPABILITIES. IN COMPENSATION THEY DO NOT NEED SO A HIGH EXPERIENCE.  SPECIFIC, DEALING IN GREAT DETAIL SOME PARTICULAR SAFETY FEATURE OR DIRECTED TO A SPECIFIC DISCIPLINE (FIRE FIGHTING, PREVENTION OF ACCIDENTS AT WORK, INSURANCE, ETC.) OR ACTIVITY (AUDITS, INSPECTIONS, COMMISSIONING, ETC.). NORMALLY THEY ARE NOT VERY USEFUL IN THE RISK ASSESSMENT. THEY MAY BE REGARDED MORE PROPERLY AS INSTRUMENTS FOR RISK MANAGEMENT.



NECESSITY OF AN ANALYTICAL AND COMPREHENSIVE ORGANIZATION OF THE LARGE (TO BE HOPED FOR) QUANTITY OF INFORMATION.

A FIRST CLUSTERING TO REDUCE THE IDENTIFIED ACCIDENTS TO POSSIBLE ACCIDENTS:

- CLUSTERING ACCORDING INITIAL EVENTS, ACCIDENTAL SEQUENCES AND TOP EVENTS
- ELIMINATION OF THE HISTORICAL ACCIDENTS NOT APPLICABLE OR NOT CREDIBLE BECAUSE OF THE SITUATION OF THE ACTUAL PLANT

THIS LEVEL OF CLUSTERING CONTRIBUTES TO BUILD UP ACCIDENT FAULT TREES, GIVING THE CONTRIBUTION OF HISTORICAL EXPERIENCE AND CHECK-LISTS (EVENTUALLY TO BE INTEGRATED WITH OTHER CONTRIBUTIONS, SUCH AS FROM STRUCTURED TECHNIQUES)



A SUBDIVISION ACCORDING THE TYPE OF INITIAL EVENT MAY BE USEFUL, AS EACH ONE MAY REQUIRE A DIFFFERENT ASSESSMENT TECHNIQUE IN THE FURTHER PHASES OF THE STUDY:

- A. ACCIDENTS DUE TO EXTERNAL NATURAL EVENTS
- B. ACCIDENTS DUE TO EXTERNAL ARTIFICIAL EVENTS
- C. ACCIDENTS DUE TO RANDOM EVENTS
- D. ACCIDENTS DUE TO PROCESS CAUSES OR HUMAN FACTORS



A SECOND CLUSTERING TO REDUCE THE POSSIBLE ACCIDENTS TO REFERENCE ACCIDENTS:

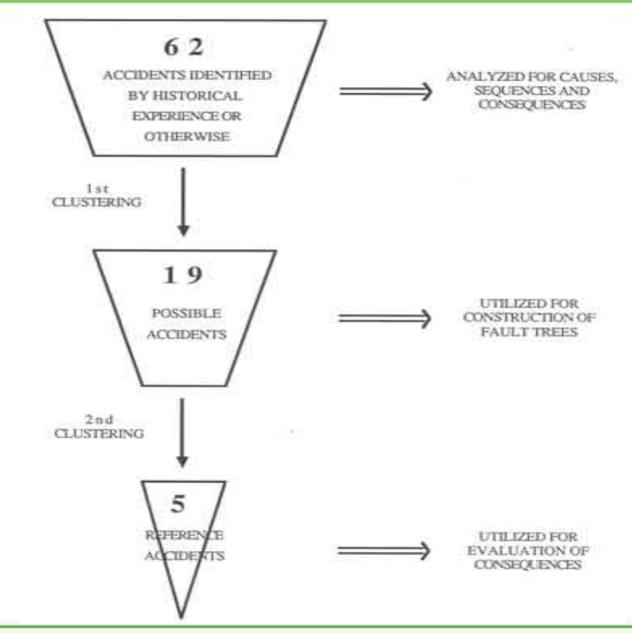
 CLUSTERING BY TYPOLOGY OF TOP EVENTS, UNIFORM BOTH PHENOMENOLOGICALLY AND QUANTITATIVELY

## THE EVALUATION OF CONSEQUENCES MAY BE CARRIED OUT LIMITING TO ANY ONE OF THE REFERENCE ACCIDENTS, DEFINED AS ABOVE.

AS AN EXAMPLE, IN THE SAFETY STUDY OF A REFINERY TANK FARM,

THE FOLLOWING DID RESULT:







THE MAIN STRUCTURED TECHNIQUES OF HAZARD IDENTIFICATION ARE:

#### \* HAZOP

#### (HAZARD AND OPERABILITY STUDY)

#### \* FMECA

(FAILURE MODE, EFFECT AND CRITICALITY ANALYSIS)

## BOTH ARE BASING ON THE TYPICAL FRAME OF A PROCESS PLANT, BASED ESSENTIALY ON TWO KIND OF ELEMENTS:

#### \* EQUIPMENT

\* PIPING



BASICALLY THEY ACT AS A SORT OF MNEMONIC KEY, TO BE EXTENSIVELY USED IN ORDER TO CENTER THE ATTENTION OF THE ANALYSTS SUCCESSIVELY ON EACH ONE OF THE ELEMENTS FORMING THE PLANT.

THE ADEQUATE APPLICATION OF SUCH TECHNIQUES REQUIRE A DEEP KNOWLEDGE OF THE PROCESS AND THE SPECIFIC FEATURES OF THE PLANT, AND A GREAT EXPERIENCE IN GENERAL ENGINEERING.

THE TECHNIQUES THEMSELVES CANNOT IN ANY WAY MAKE UP THE LACK OF EXPERIENCE OR SPECIFIC KNOWLEDGE.



# THE COMPONENTS OF THE TEAM WILL BE, AS A MINIMUM:

- \* AN EXPERT IN THE APPLICATION OF THE METHODOLOGY
- \* A PROCESS ENGINEER
- \* AN EXPERT IN OPERATION/MAINTENANCE
- \* EVENTUAL SPECIALISTS (PART TIME)



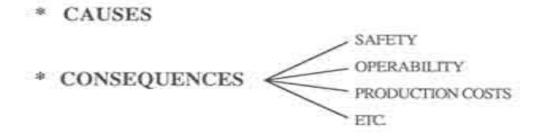
#### HAZOP

(HAZard and OPerability study)

## ANALYZES THE PLANT LINE BY LINE, EQUIPMENT BY EQUIPMENT, TAKING IN CONSIDERATION FOR EACH ONE OF THESE ELEMENTS:

\* INTENTIONS

\* DEVIATIONS



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BY APPLYING TO:



\* ACTIVITY

\* SUBSTANCES

\* PHASES

(\* TIME)

- (\* PLACE)
- (\* REASON)



## PRIMARY RESULTS

## OF A HAZOP ANALYSIS:

# \* INTERVENTIONS AND MODIFICATIONS TO BE MADE TO INCREASE THE LEVEL OF SAFETY, OPERABILITY, ETC.

# \* IDENTIFICATION OF THE POSSIBLE ACCIDENTAL EVENTS, TO BE FURTHER ANALYZED IN THE NEXT STEPS.



#### OTHER POSSIBLE RESULTS:

\* INDICATION, FOR ANY ANALYTICAL STEP, OF THE POSSIBLE EVENTS ACTUALLY MEANINGFUL.

\* GROUPING OF THE EVENTS, TO SHOW THE POSSIBLE DIFFERENT SEQUENCES LEADING TO A STATED ACCIDENT.

\* LOGICAL SYNTHESIS (CLUSTERING) OF THE VARIOUS POSSIBLE ACCIDENTAL SEQUENCES IN ORDER TO ENABLE THE DRAWING OF THE COMPLETE FAULT TREE.



#### PRELIMINARY HAZARD ANALYSIS

#### (PHA)

- LIST OF RISK TYPOLOGIES
- LIST AND LAY-OUT OF HAZARDOUS SUBSTANCES AND/OR EQUIPMENT, PER EACH TYPOLOGY OF RISK
- ANALYSIS CAUSES/CONSEQUENCES/ ACTIONS

#### EXAMPLE

RISK:

- RELEASE OF FLAMMABLE MATERIAL

H<sub>2</sub>S

SO2

TO

- CONFINED EXPLOSION
- RELEASE OF TOXIC MATERIAL HF
- RUNAWAY REACTION
- ETC.

Egyptian and Italian Quantitative

Egyptian and Italian Cooperation Programme on Environment Quantitative Risk Assessment of Oil and Gas Plants

COMPARATIVE APPLICATIONS, TO SHOW THE DIFFERENT COMPLETENESS THAT THE VARIOUS TECHNIQUES OF HAZARD IDENTIFICATION MAY OFFER.

DEPENDING ON THE PERSPECTIVE, THE RESULTS OF SUCH AN ANALYSIS MAY DIFFER, AS THREE DIFFERENT TYPE OF INFORMATION MAY BE TAKEN INTO ACCOUNT:

ACCIDENTAL EVENTS

- DEVIATIONS OR INITIATING CAUSES

CONTROL ACTIONS



AS A GENERAL EXPERIENCE (GAINED IN A NUMBER OF APPLICATIONS):

#### DEGREE OF COMPLETENESS ACHIEVABLE BY A HAZOP PERFORMED IN DETAIL: (1-3 DAYS / P&I)

#### 70-80% FOR CONTINUOUS PROCESSES 50-60% FOR BATCH PROCESSES

## DEGREE OF COMPLETENESS ACHIEVABLE BY A HAZOP PERFORMED ACCORDING A LOWER STANDARD:

(2-4 HOURS / P&I)

#### IDENTIFIABLE

2/3 OF ACCIDENTAL EVENTS 1/3 OF DEVIATIONS AND ACTIONS

- WITH RESPECT TO THE ONES OBTAINED
- BY A DETAILED HAZOP.